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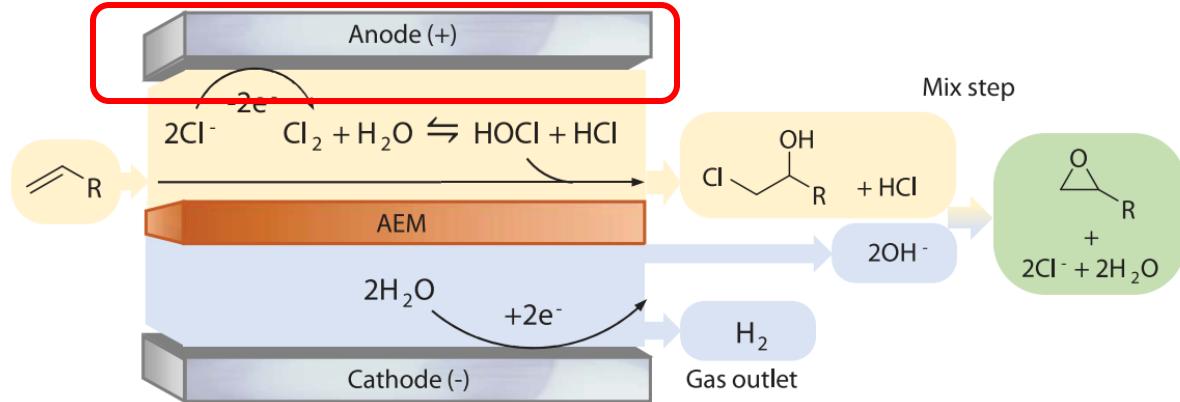
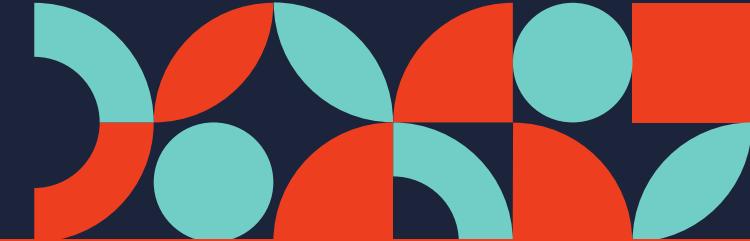
October 27 – 31, 2024
San Diego Convention Center
Hilton San Diego Bayfront

Tuning Chlorine vs Oxygen Evolution on Graphene Supported Single Atom Electrocatalysts

Richard Tran

CHEMICAL ENGINEERING REIMAGINED

Decoupling CER from OER

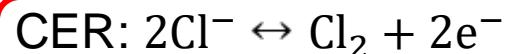


Ethylene/propylene oxide and H_2 production from CER

Leow, W. R. et. al. (2020). *Science*, 368(6496), 1228–1233. <https://doi.org/10.1126/science.aaz8459>



$$U_{\text{OER}}^0 = 1.23 \text{ V vs SHE}$$

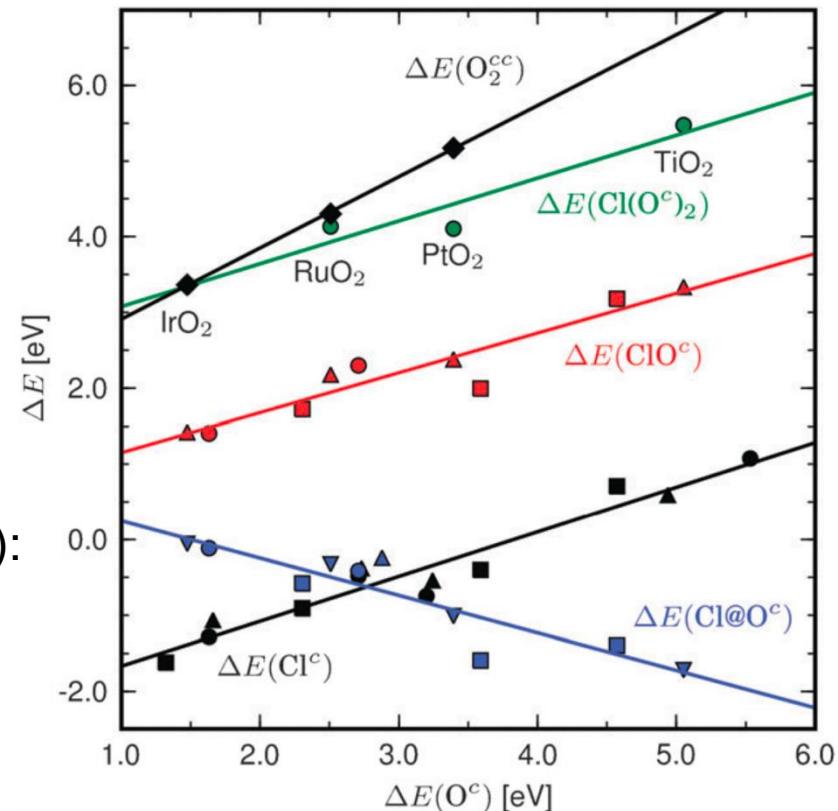


$$U_{\text{CER}}^0 = 1.36 \text{ V vs SHE}$$

Typical electrocatalysts, dimensionally stable anodes (DSA):

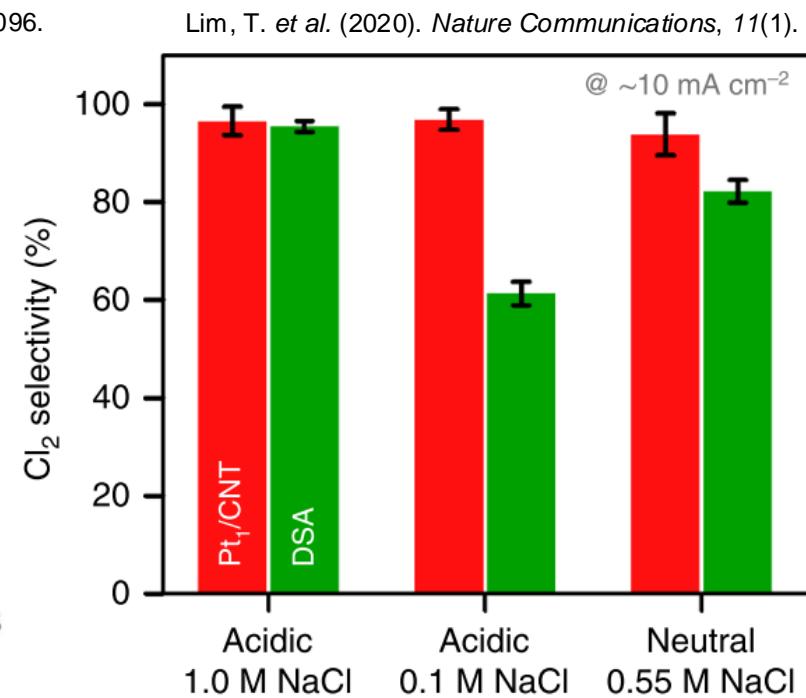
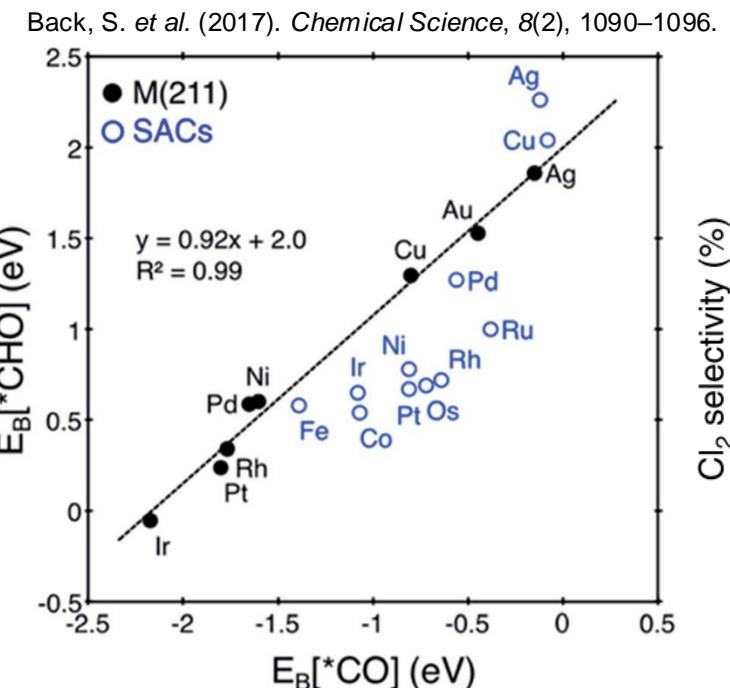
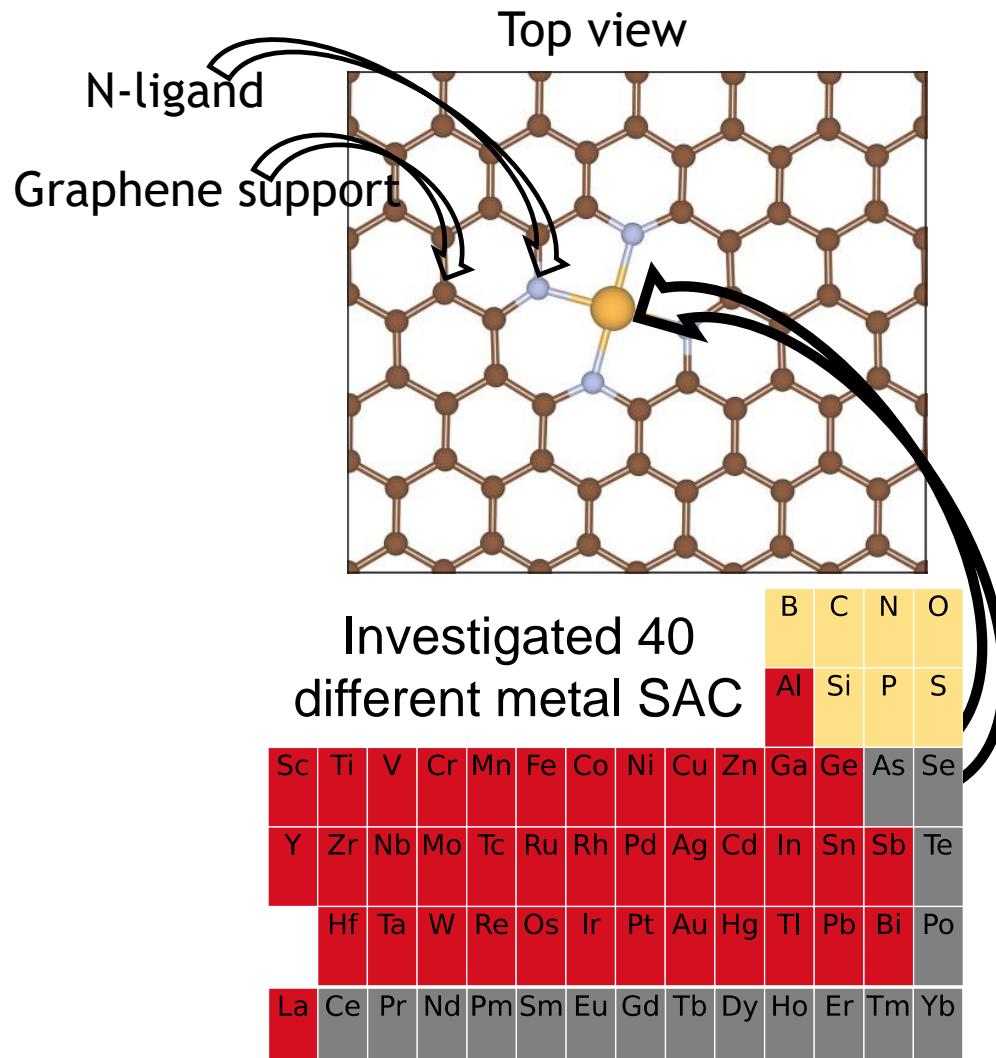
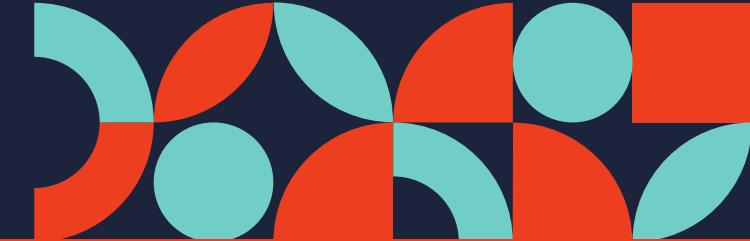
	$\eta_{\text{OER}} (\text{V})$	$\eta_{\text{CER}} (\text{V})$
RuO_2	0.2-0.4	0.0-0.1
IrO_2	0.4-0.6	0.2-0.4

Hansen, H. A., et al. (2010). *Physical Chemistry Chemical Physics*, 12(1), 283–290. <https://doi.org/10.1039/b917459a>



OER and CER are coupled on oxide catalysts
→ prevents independent tuning/selectivity

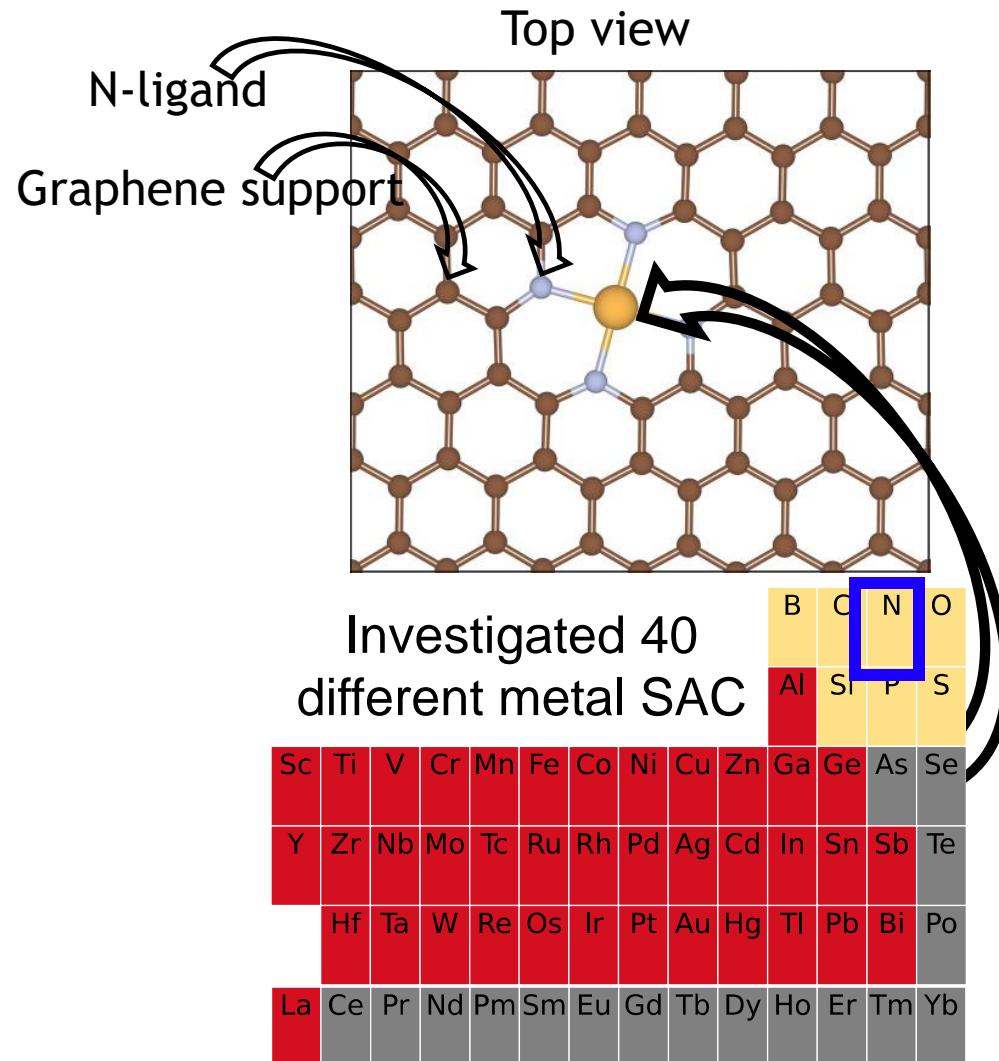
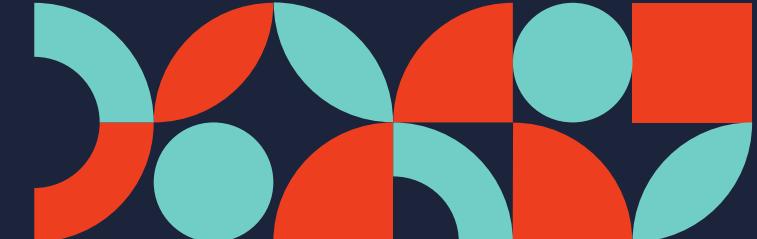
Graphene supported SACs



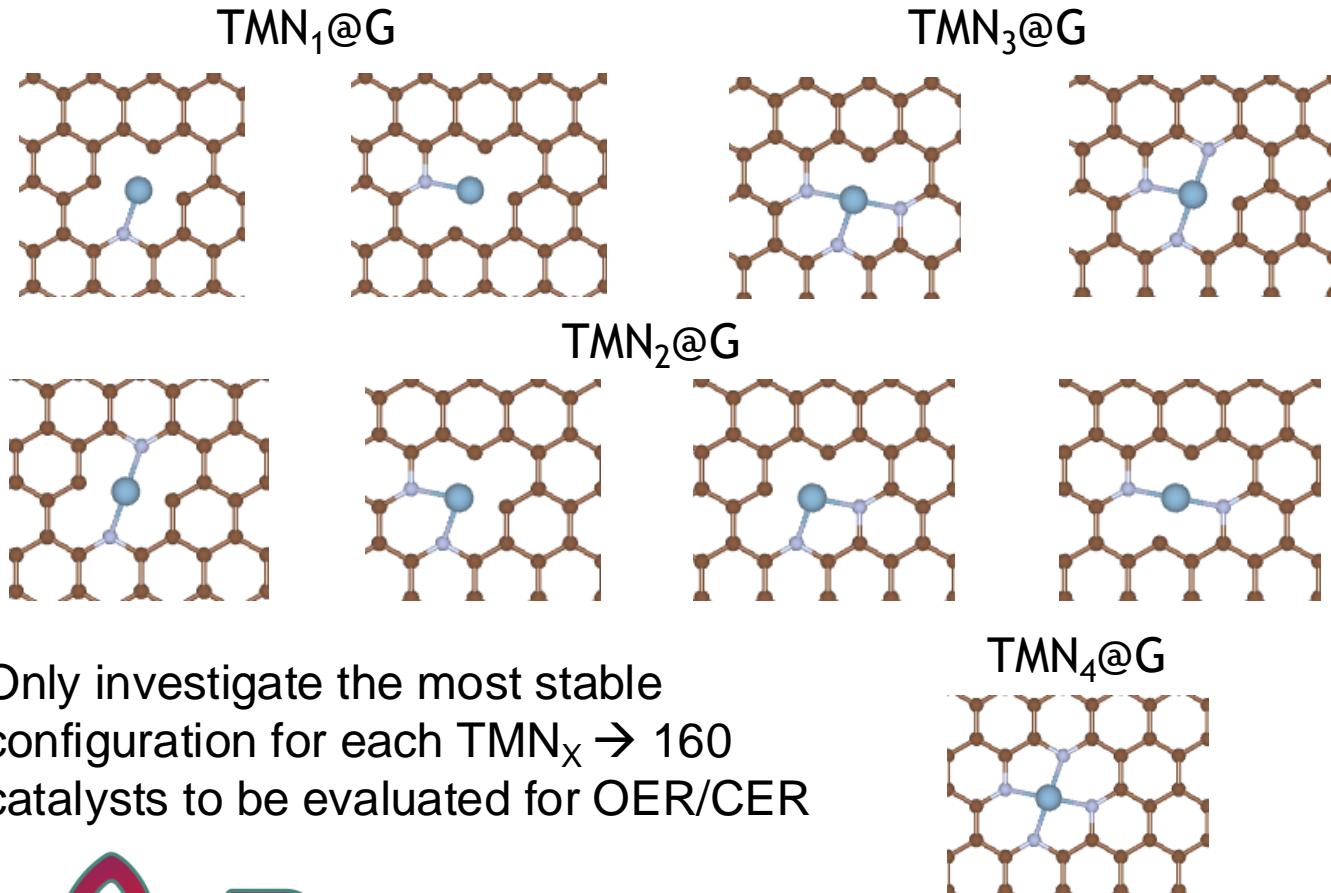
SACs demonstrate different scaling relationships when compared to metal surfaces and oxides for different reactions

Pt SACs improve selectivity relative to DSAs across different pH conditions

DFT simulations

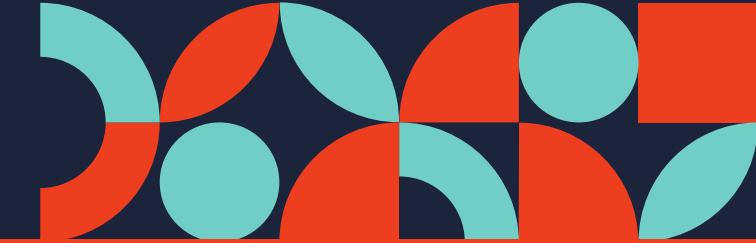


VASP



- 14.8 Å x 12.8 Å sheet
- GGA PBE w/ BEEF-vdW
- K-points: 6 x 6 x 1

CER/OER intermediates



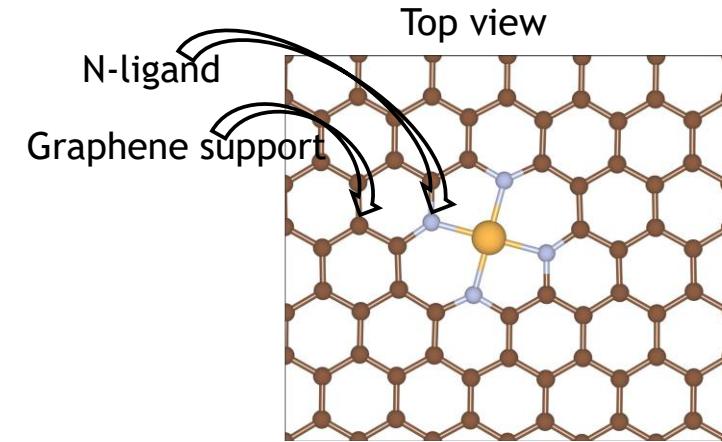
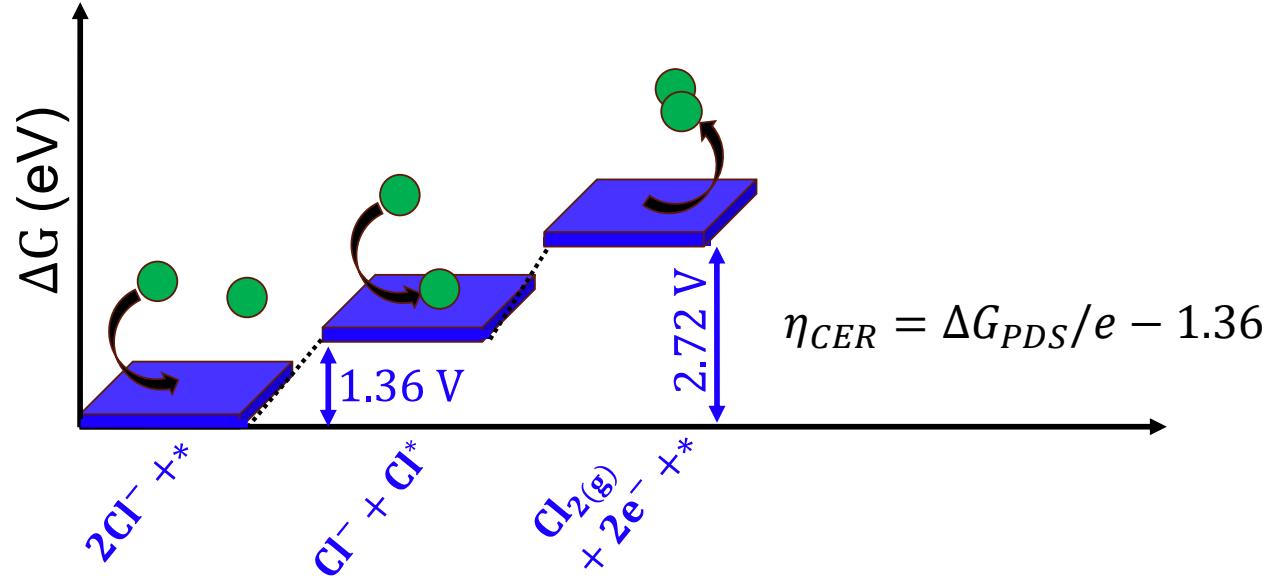
$$U_{CER}^0 = 1.36 \text{ V vs SHE},$$

$$2U_{CER}^0 = 2.72 \text{ V}$$

$$G_{\text{corr}} = \Delta ZPE - T\Delta S^o$$

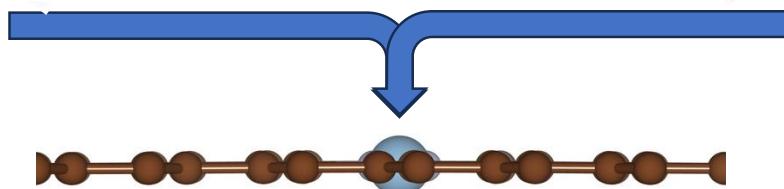
$$\mu_{Cl} = \frac{1}{2} G_{Cl_2(g)} + \ln(a_{Cl^-})k_B T - eU + 1.36$$

The Volmer-Heyrovsky mechanism



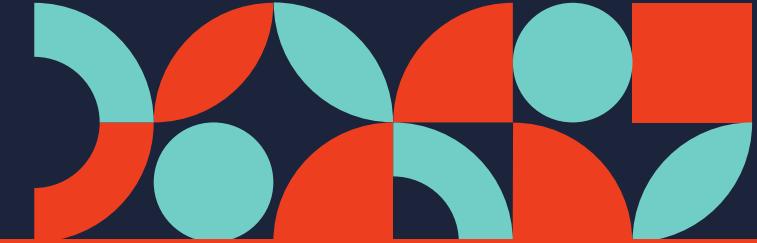
Calculated 5 adsorbates

Cl^*



Side view

CER/OER intermediates



$$U_{OER}^0 = 1.23 \text{ V vs SHE},$$

$$4U_{OER}^0 = 4.92 \text{ V}$$

$$G_{\text{corr}} = \Delta ZPE - T\Delta S^o$$

$$\mu_{H_2} = G_{H_2(g)} - 2(k_B T p H \ln(10) - eU)$$

$$\Delta G_1 = E_{HO^*} + \frac{1}{2}\mu_{H_2} - \mu_{H_2O(l)} - E^* + G_{\text{corr}}$$

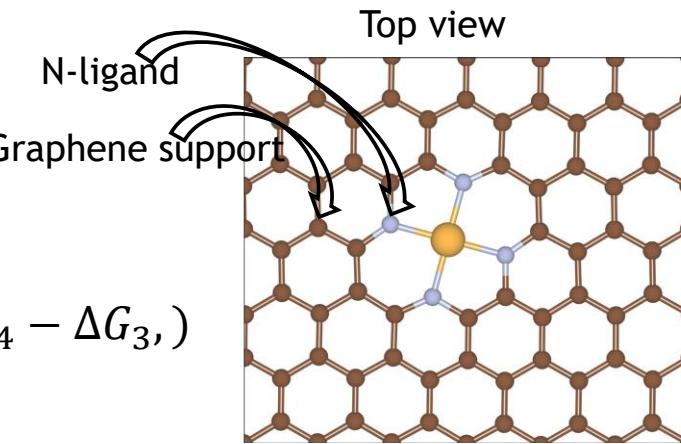
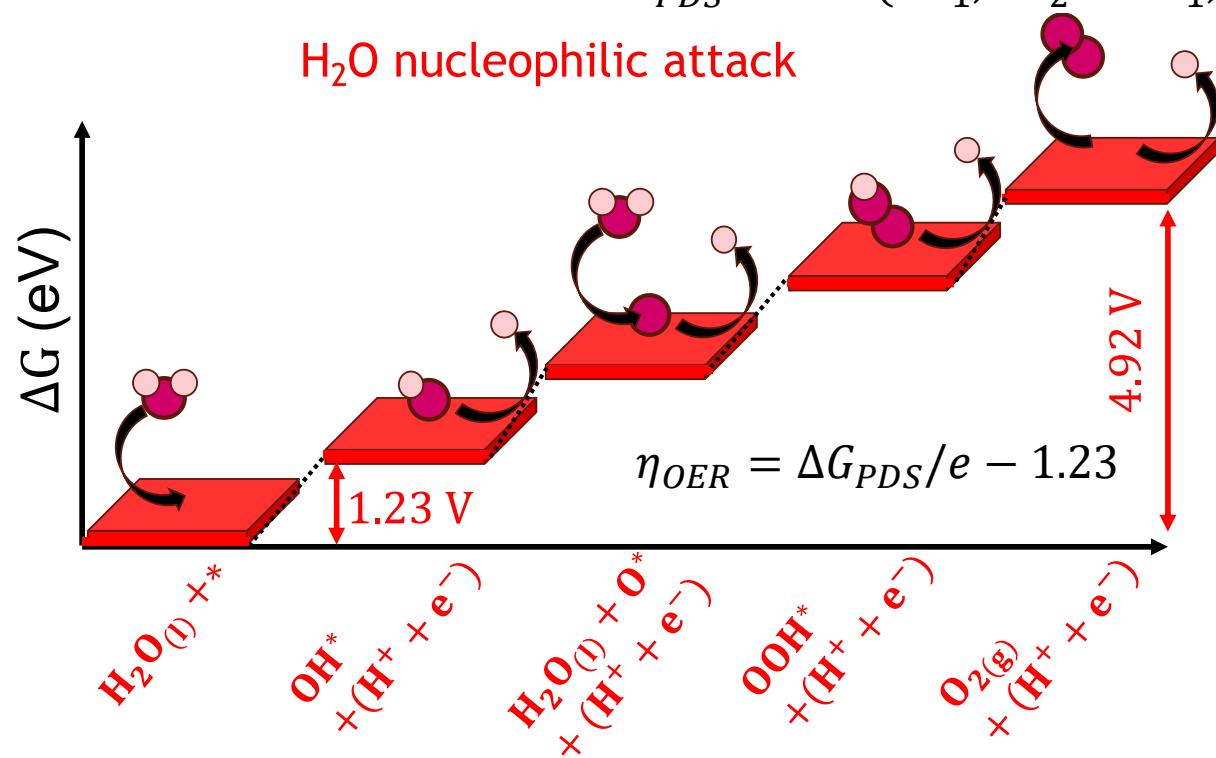
$$\Delta G_2 = E_{O^*} + \mu_{H_2} - \mu_{H_2O(l)} - E^* + G_{\text{corr}}$$

$$\Delta G_3 = E_{OOH^*} + \frac{3}{2}\mu_{H_2} - 2\mu_{H_2O(l)} - E^* + G_{\text{corr}}$$

$$\Delta G_4 = 2\mu_{H_2} - 2\mu_{H_2O(l)}$$

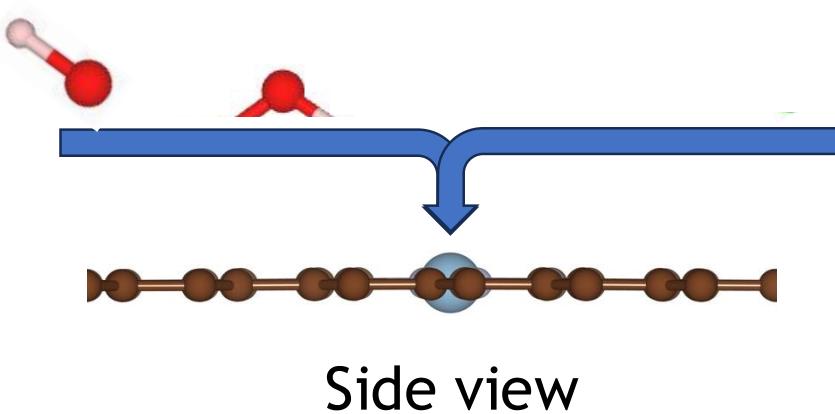
$$\Delta G_{PDS} = \max(\Delta G_1, \Delta G_2 - \Delta G_1, \Delta G_3 - \Delta G_2, \Delta G_4 - \Delta G_3)$$

H₂O nucleophilic attack

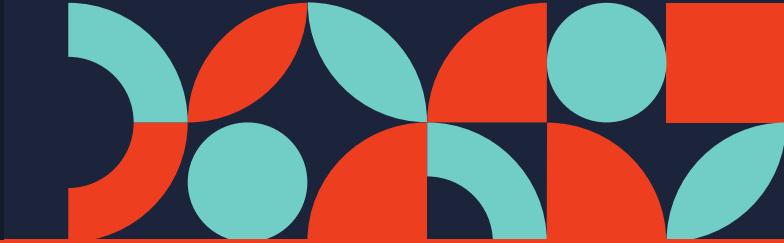


Calculated 5 adsorbates

OH* OOH* O* Cl*



CER/OER intermediates



$$U_{CER}^0 = 1.36 \text{ V vs SHE},$$

$$2U_{CER}^0 = 2.72 \text{ V}$$

$$G_{\text{corr}} = \Delta ZPE - T\Delta S^o$$

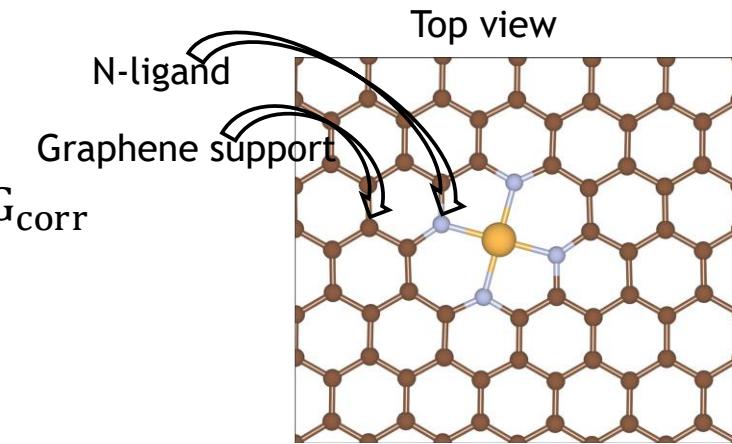
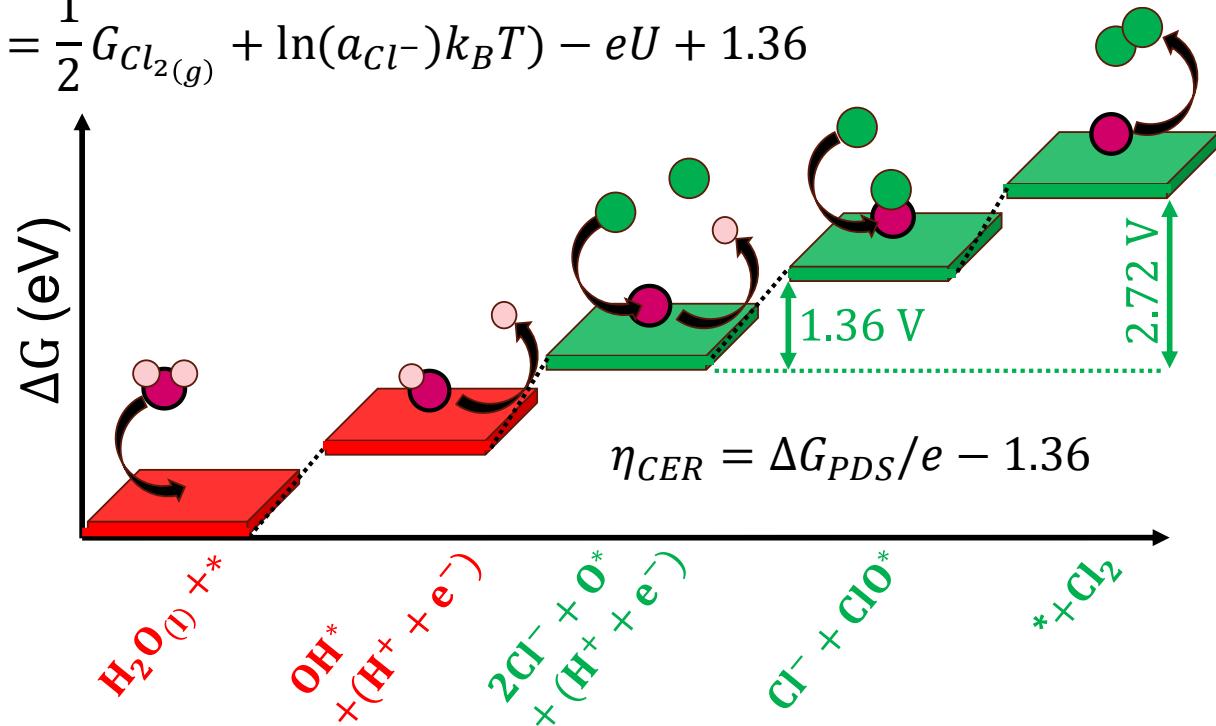
$$\Delta G_1 = E_{O^*} + \mu_{H_2} - \mu_{H_2O(l)} - E^* + G_{\text{corr}}$$

$$\Delta G_2 = E_{ClO^*} - \mu_{H_2} - \mu_{H_2O(l)} - \mu_{Cl} - E^* + G_{\text{corr}}$$

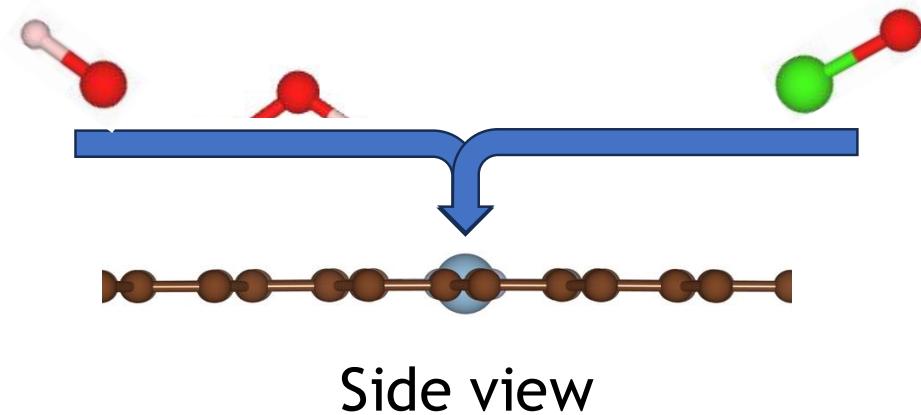
$$\Delta G_3 = E_{O^*} + \mu_{Cl_2} + \mu_{H_2} - \mu_{H_2O(l)} - E^* - 2\mu_{Cl} + G_{\text{corr}}$$

$$\Delta G_{RDS} = \max(\Delta G_2 - \Delta G_1, \Delta G_3 - \Delta G_2)$$

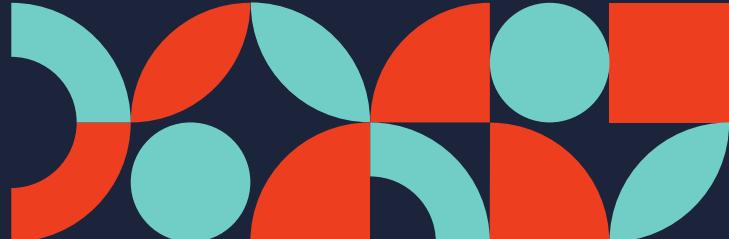
$$\mu_{Cl} = \frac{1}{2} G_{Cl_2(g)} + \ln(a_{Cl^-})k_B T) - eU + 1.36$$



Calculated 5 adsorbates
 OH^* OOH^* O^* Cl^* ClO^*



Scaling relationships

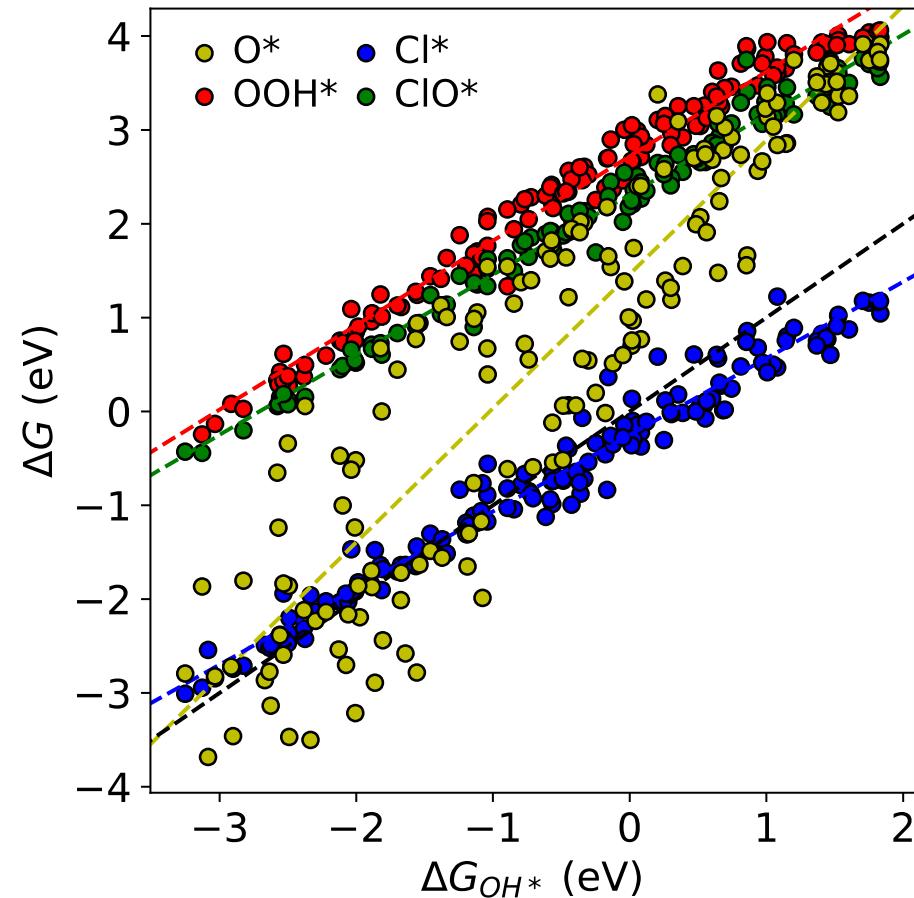


$$\Delta G_{O^*} = 1.4 \Delta G_{OH^*} + 1.5$$

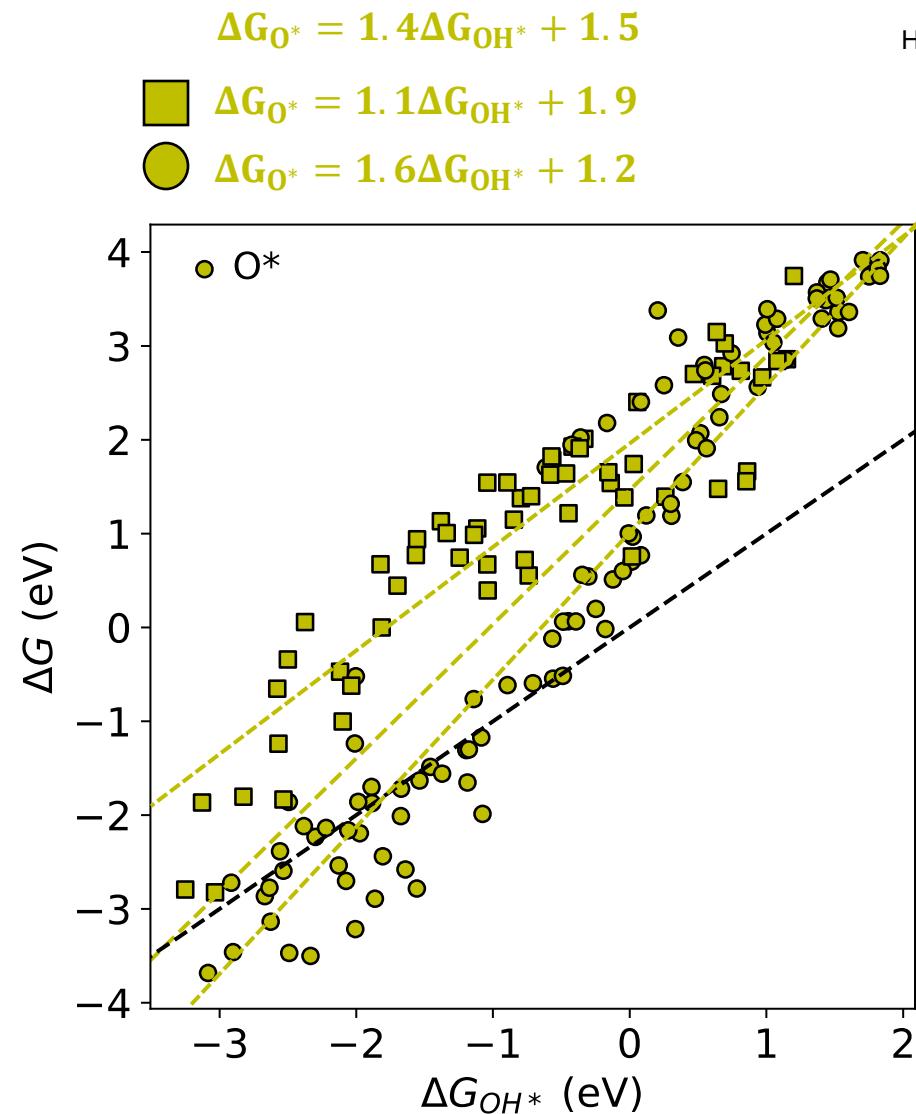
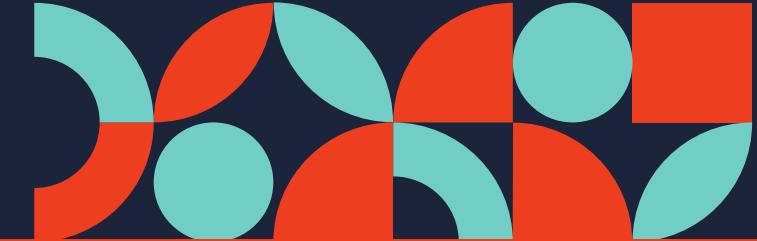
$$\Delta G_{OOH^*} = 0.9 \Delta G_{OH^*} + 2.7$$

$$\Delta G_{ClO^*} = 0.9 \Delta G_{OH^*} + 2.3$$

$$\Delta G_{Cl^*} = 0.8 \Delta G_{OH^*} - 0.2$$

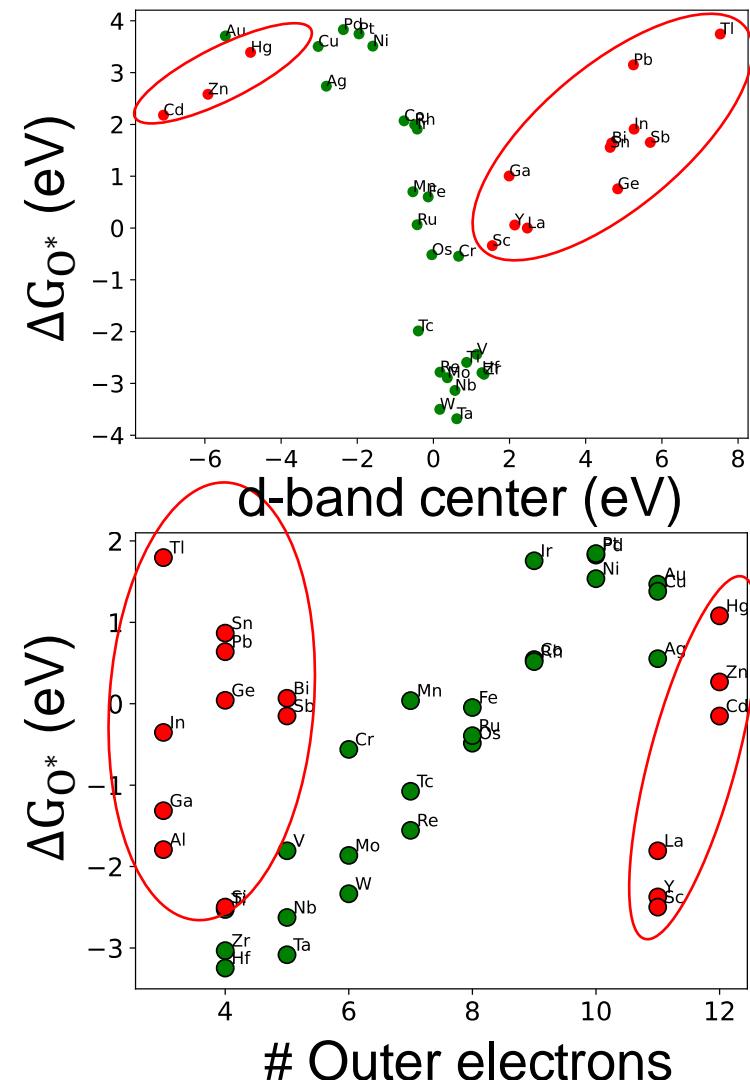


Scaling relationships



H. Xin, S. Linic, J. Chem. Phys. 132 (2010) 221101

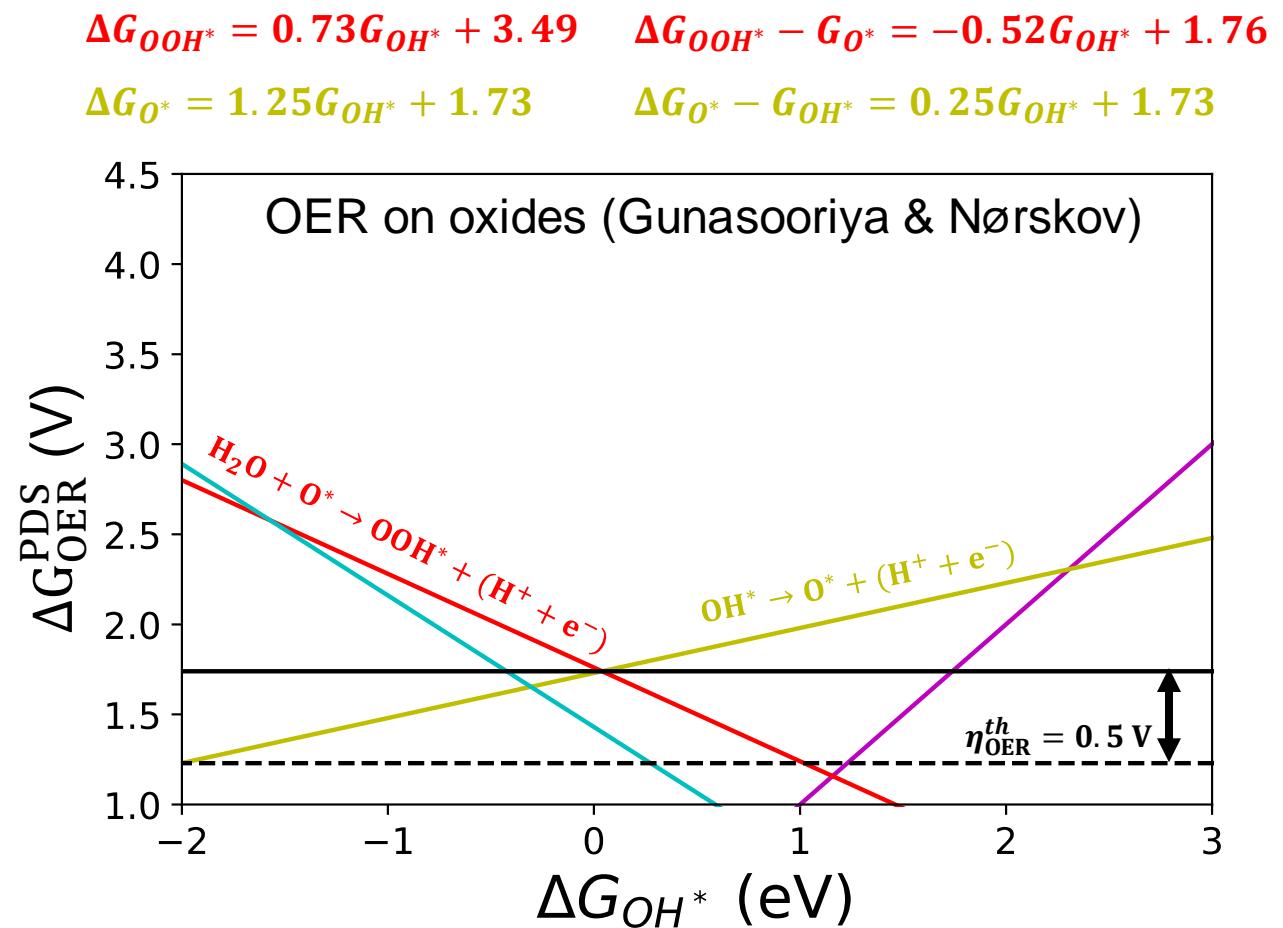
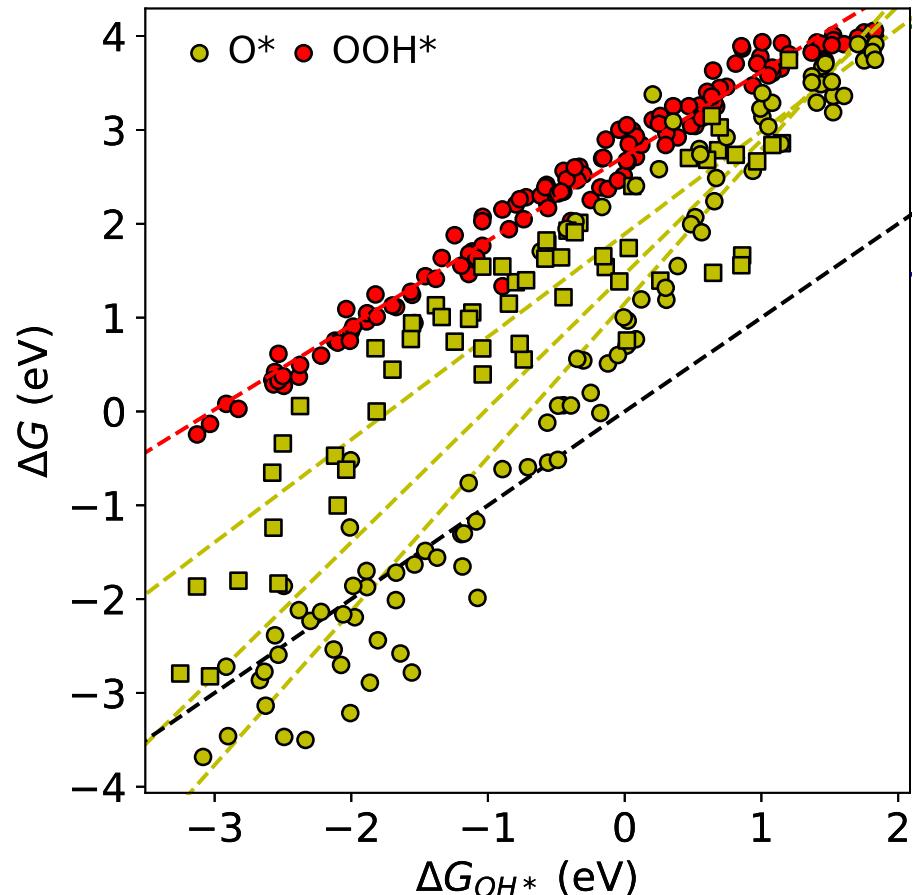
Sc	Ti	V	Cr	Mn	Fe	Co	Ni	Cu	Zn	Al	Si	Ge	P
Y	Zr	Nb	Mo	Tc	Ru	Rh	Pd	Ag	Cd	In	Sn	Sb	
	Hf	Ta	W	Re	Os	Ir	Pt	Au	Hg	Tl	Pb	Bi	
La	Ce	Pr	Nd	Pm	Sm	Eu	Gd	Tb	Dy	Ho	Er	Tm	



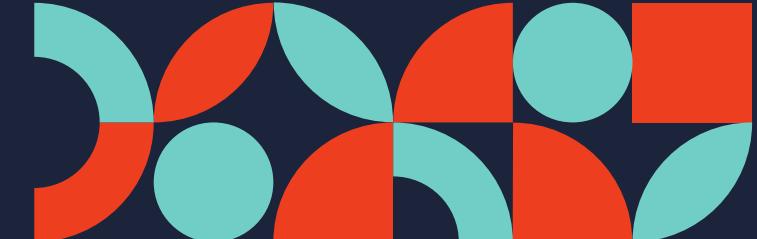
Sabatier principle



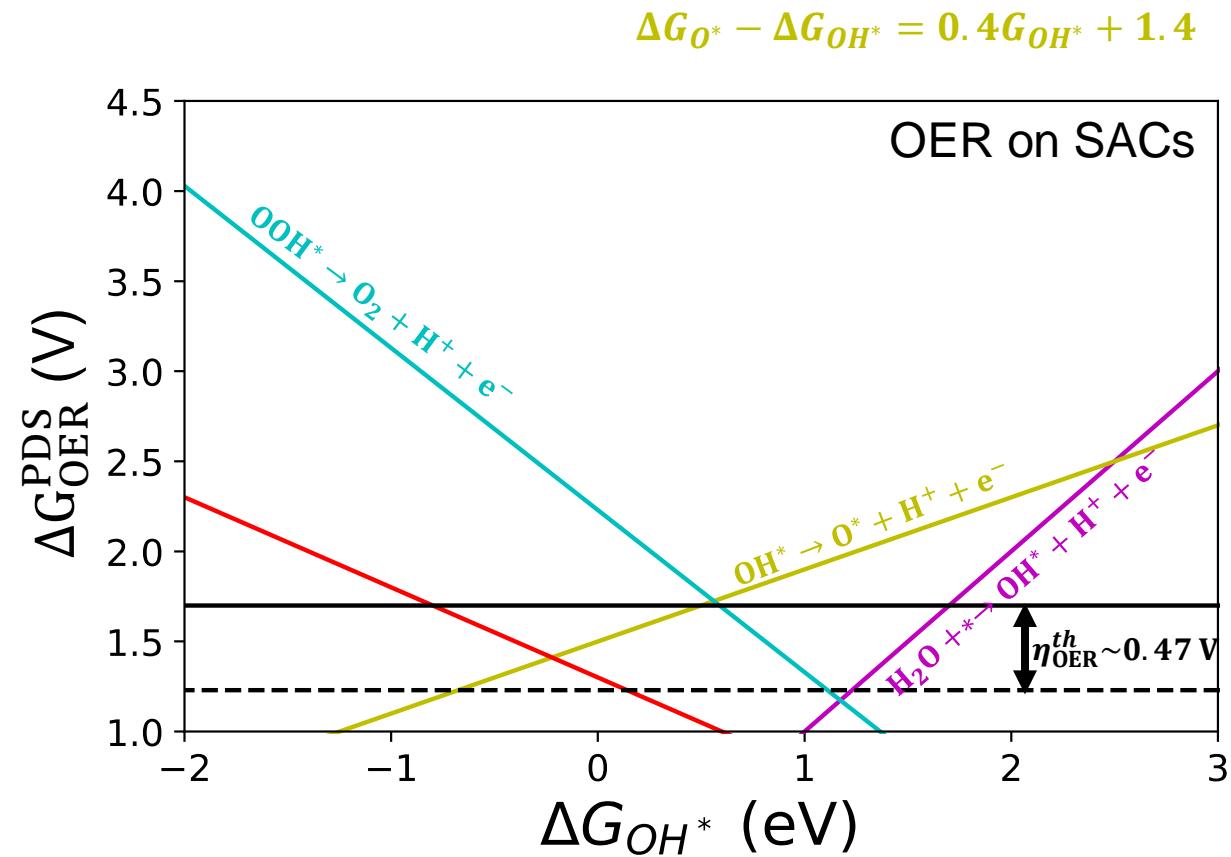
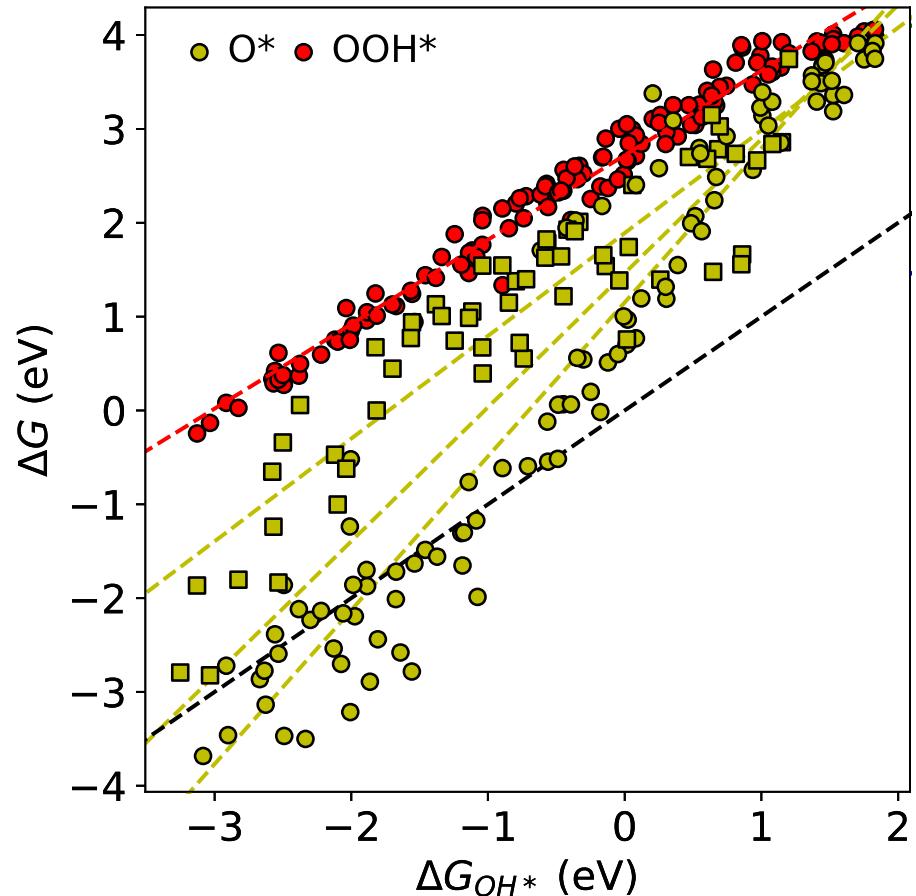
Gunasooriya, G. T. K. K., & Nørskov, J. K. (2020). *ACS Energy Letters*, 5(12), 3778–3787. <https://doi.org/10.1021/acsenergylett.0c02030>



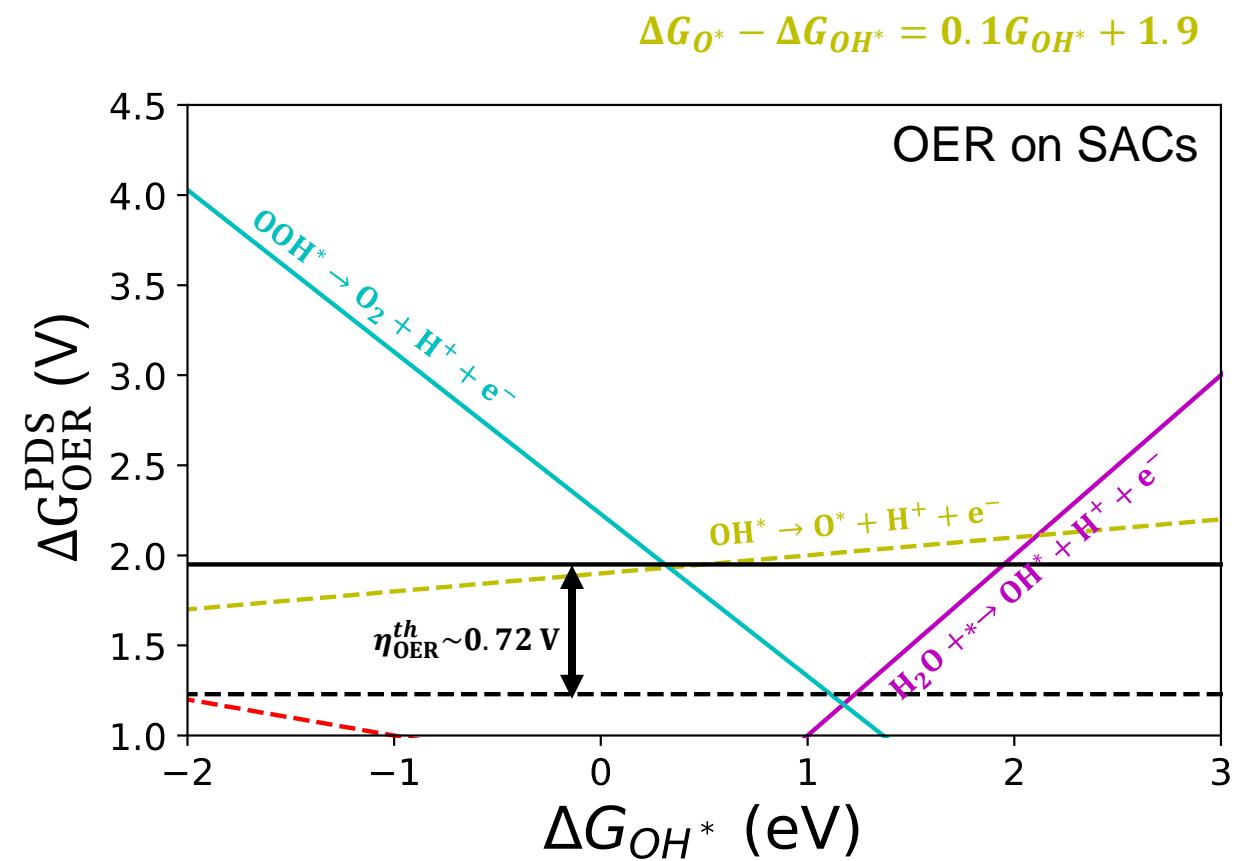
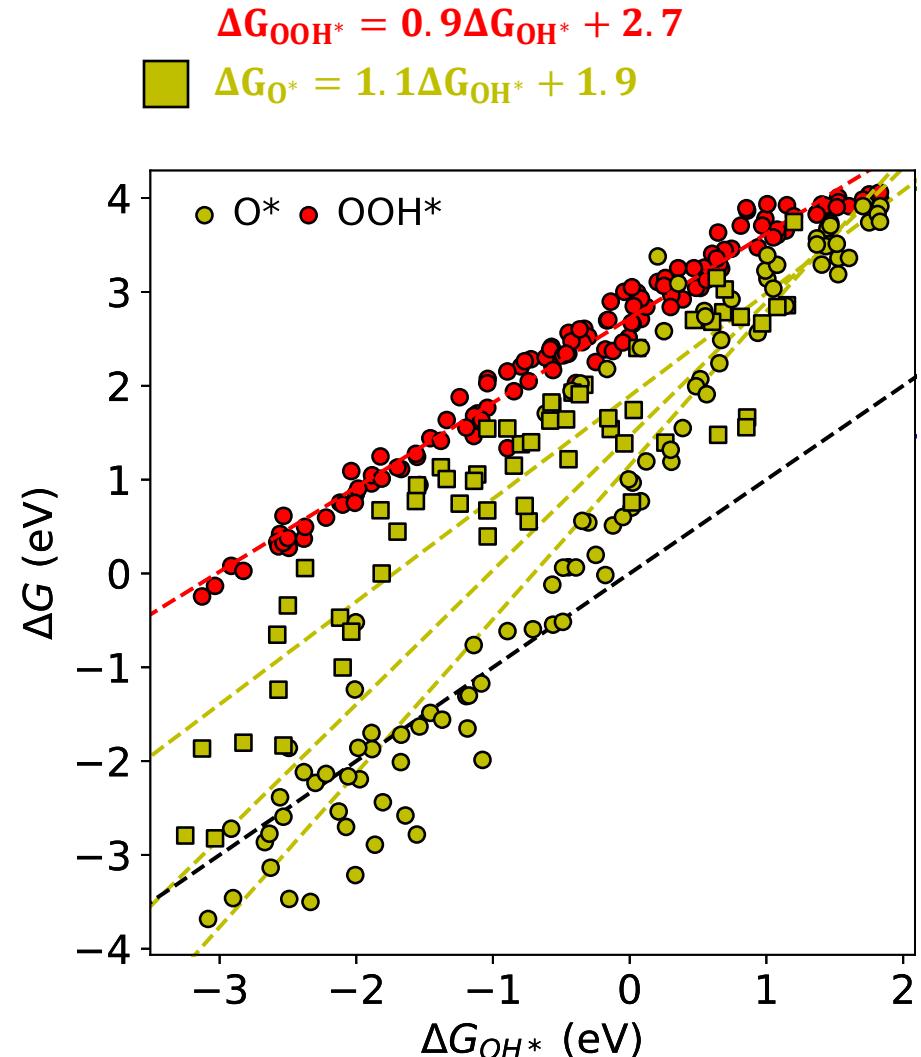
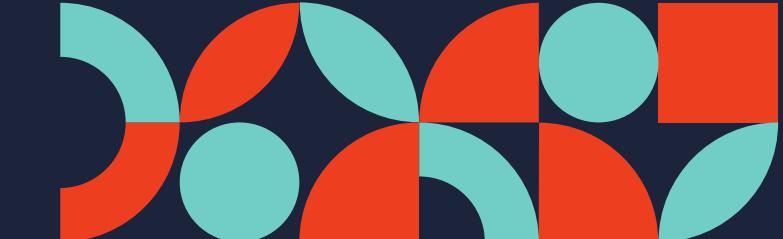
Sabatier principle



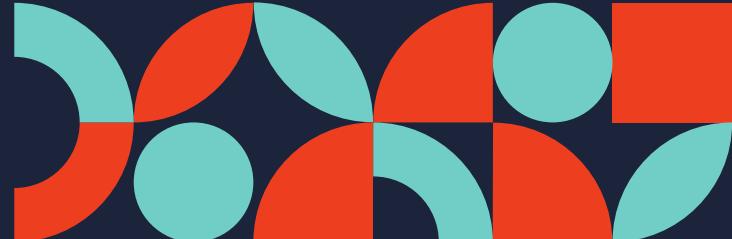
$$\Delta G_{O^*} = 1.4 \Delta G_{OH^*} + 1.5$$
$$\Delta G_{OOH^*} = 0.9 \Delta G_{OH^*} + 2.7$$



Sabatier principle

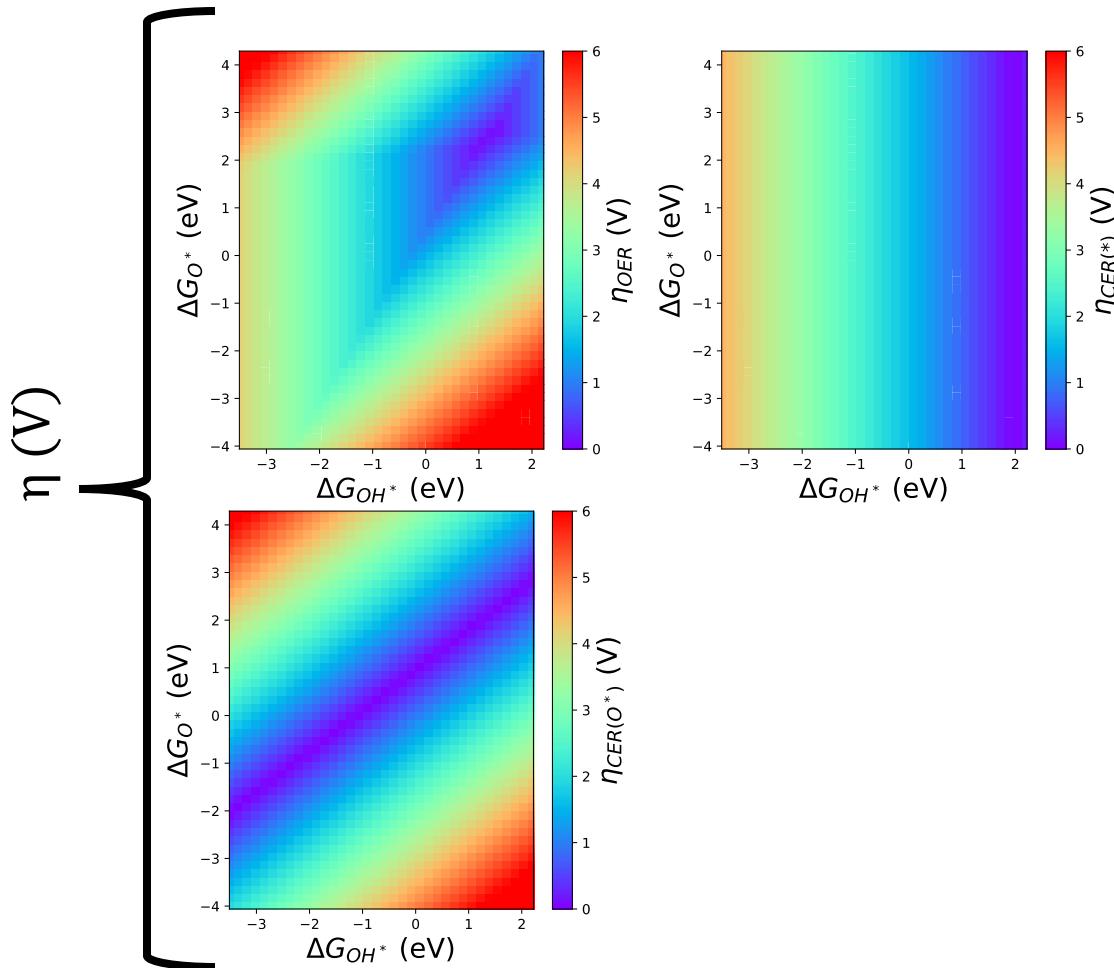
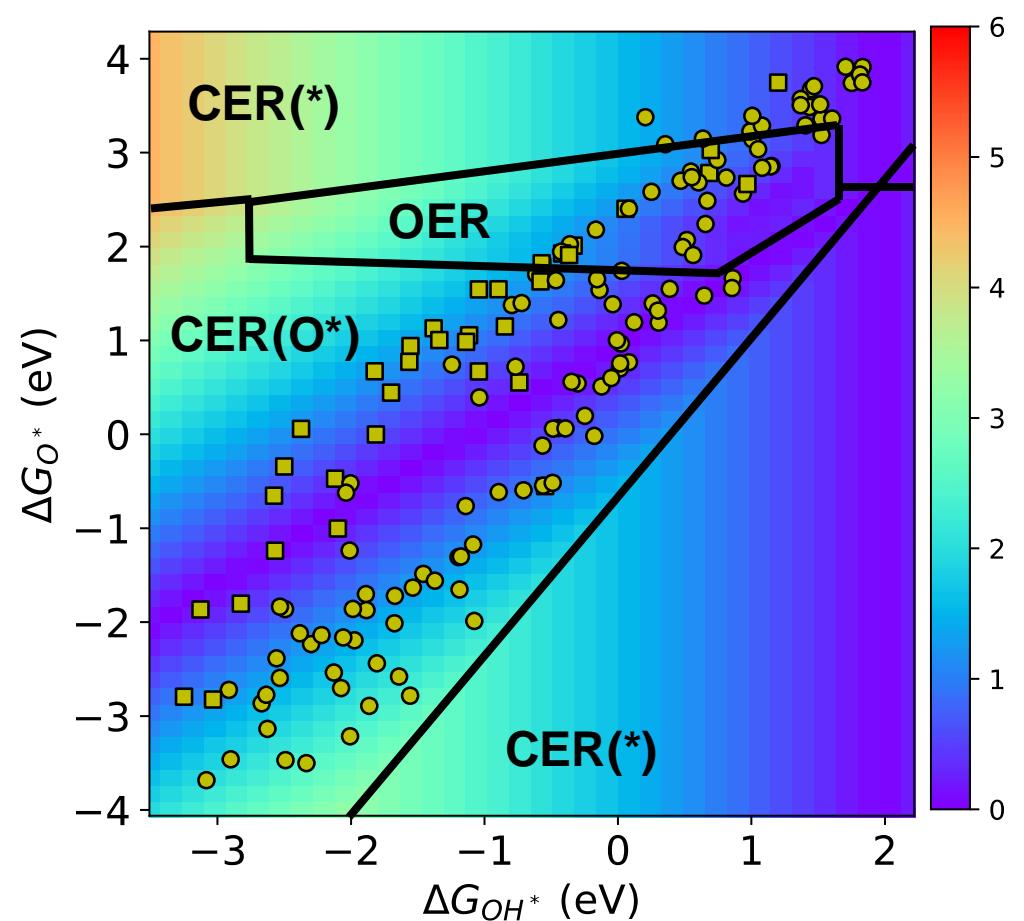


Selectivity and activity

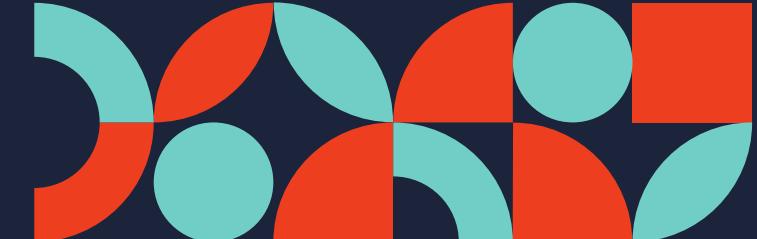


$$sel = (U_{OER}^0 + \eta_{TD(OER)}) - (U_{CER}^0 + \eta_{TD(CER)})$$

$sel > 0 \rightarrow \text{CER}$, $selectivity < 0 \rightarrow \text{OER}$

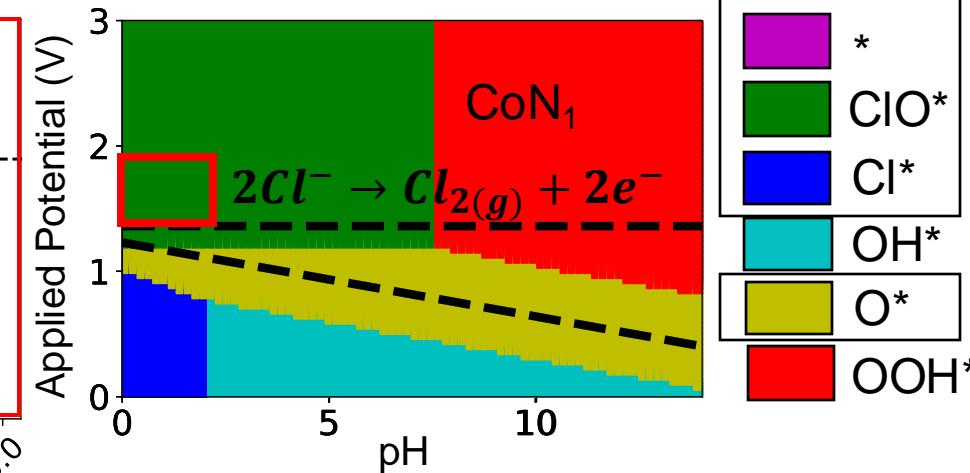
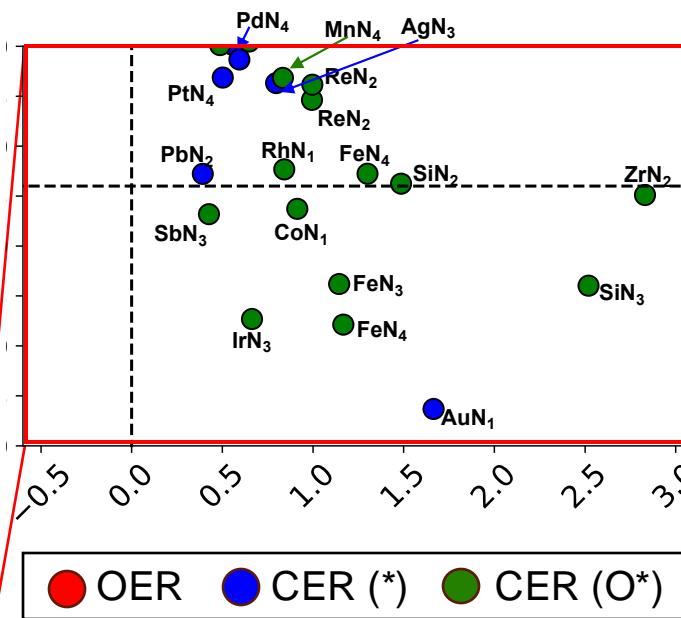
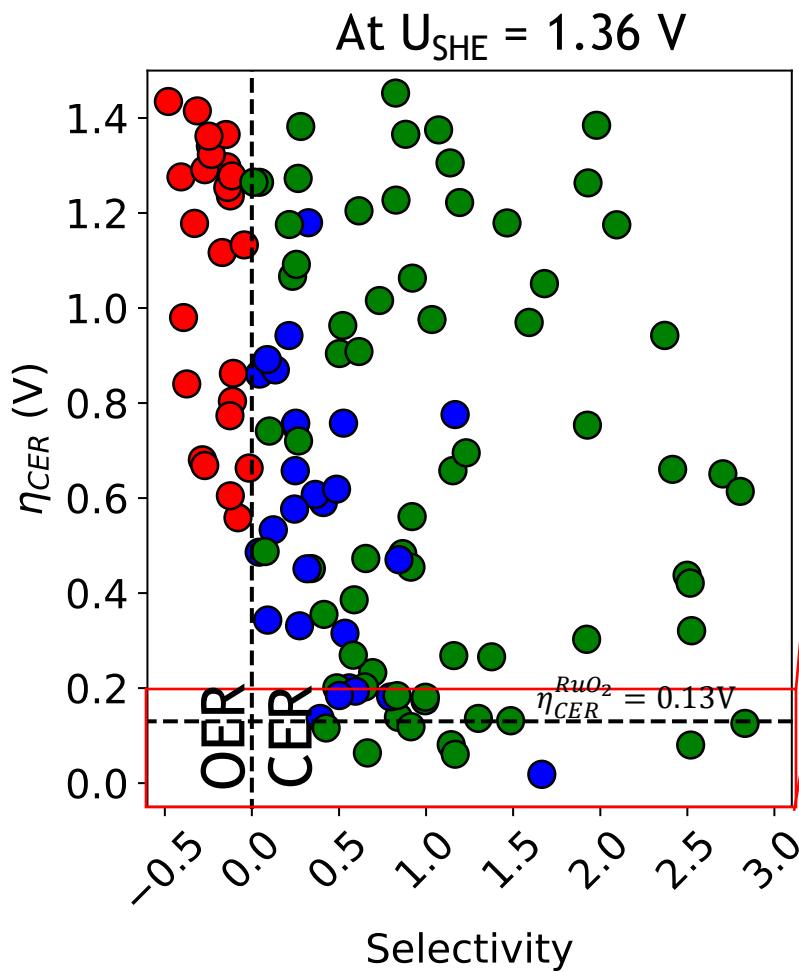


Candidate catalysts CER

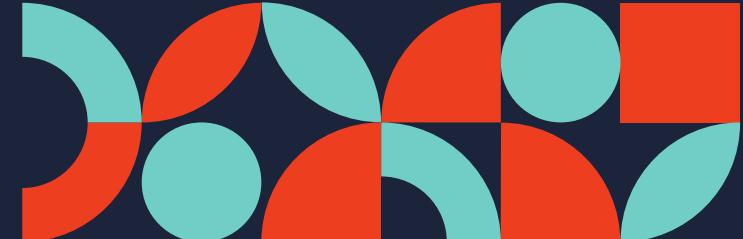


$$sel = (U_{OER}^0 + \eta_{TD(OER)}) - (U_{CER}^0 + \eta_{TD(CER)})$$

$sel > 0 \rightarrow \text{CER}, selectivity < 0 \rightarrow \text{OER}$

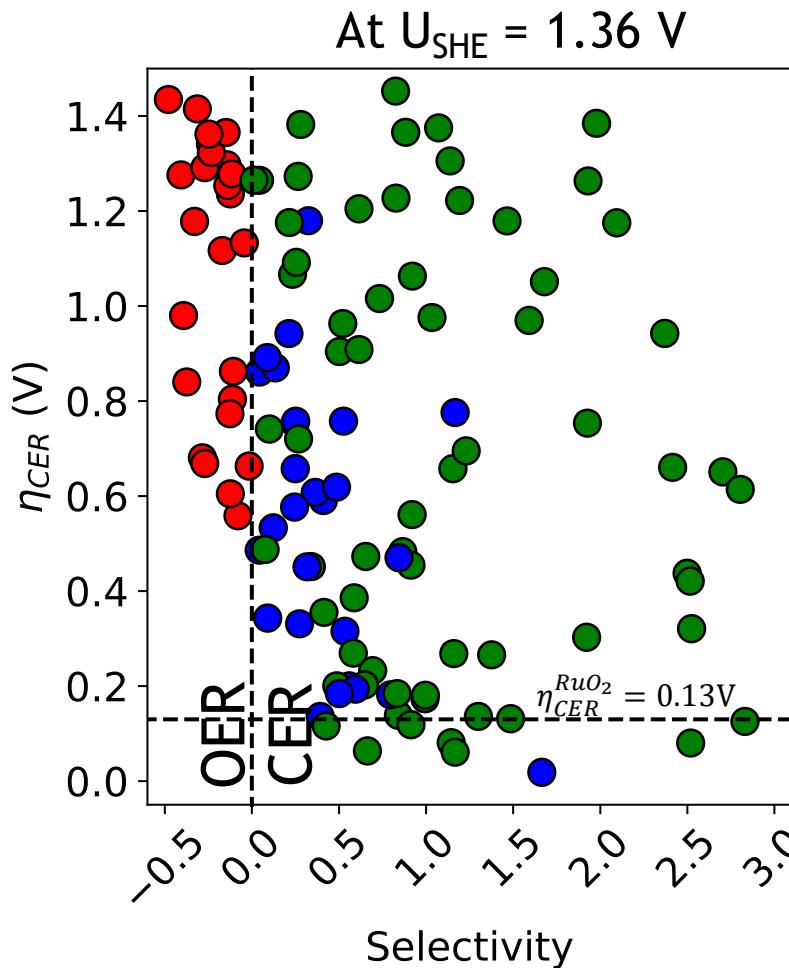


Candidate catalysts CER



$$sel = (U_{OER}^o + \eta_{TD(OER)}) - (U_{CER}^o + \eta_{TD(CER)})$$

$sel > 0 \rightarrow \text{CER}, selectivity < 0 \rightarrow \text{OER}$

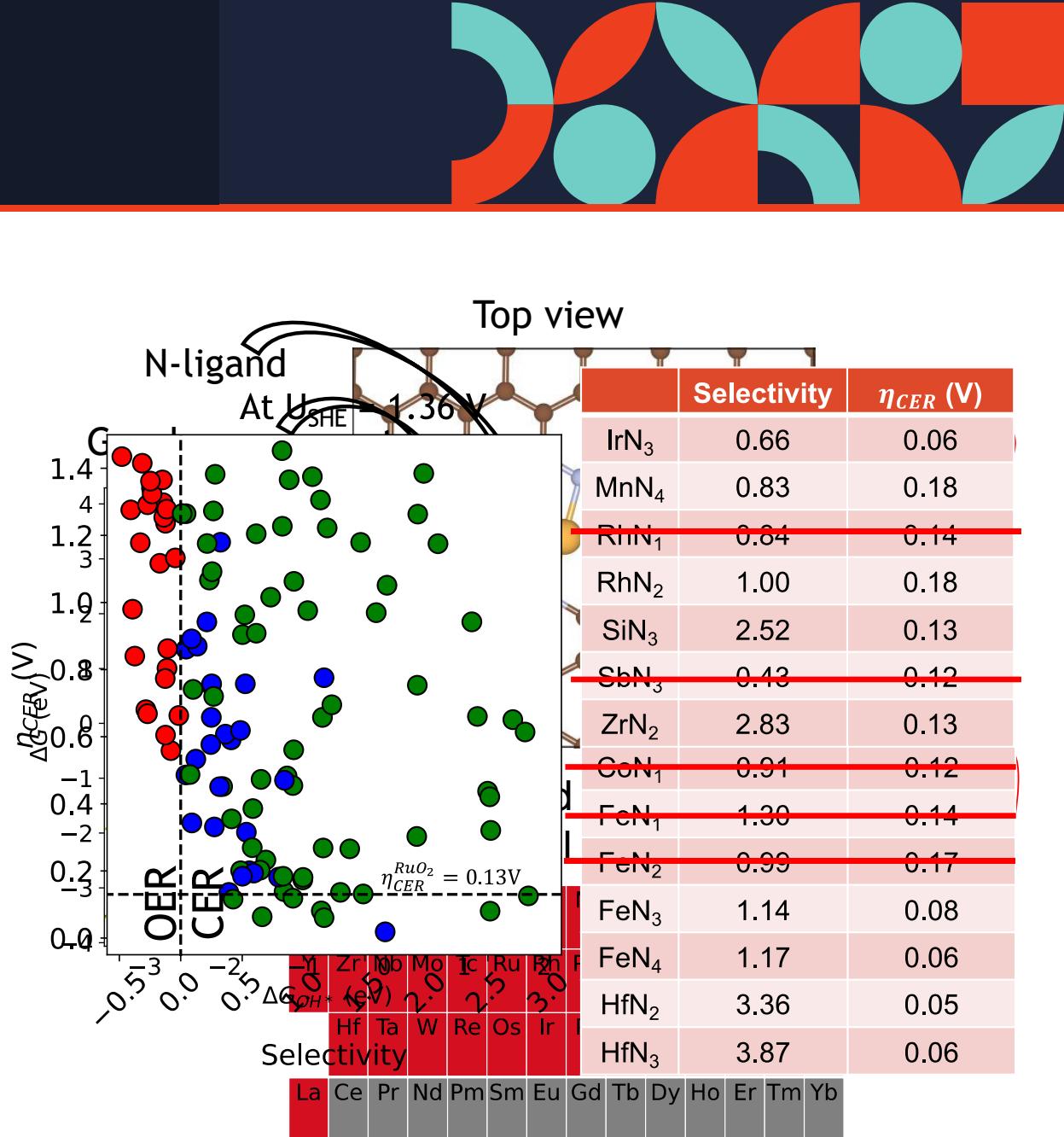


	Selectivity	$\eta_{CER} (\text{V})$
CoN ₁	0.91	0.12
FeN ₁	1.30	0.14
FeN ₂	0.99	0.17
FeN ₃	1.14	0.08
FeN ₄	1.17	0.06
HfN ₂	3.36	0.05
HfN ₃	3.87	0.06

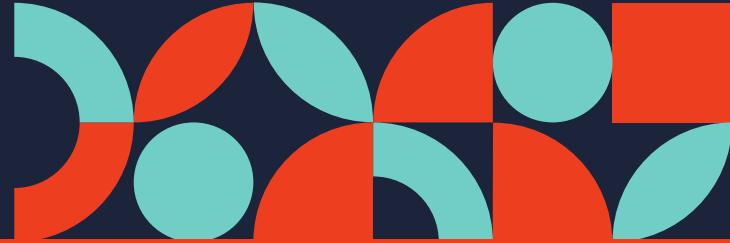
	Selectivity	$\eta_{CER} (\text{V})$
IrN ₃	0.66	0.06
MnN ₄	0.83	0.18
RhN ₁	0.84	0.14
RhN ₂	1.00	0.18
SiN ₃	2.52	0.13
SbN ₃	0.43	0.12
ZrN ₂	2.83	0.13

Conclusion

- Evaluated CER vs OER for 160 SACs ($MN_x@G$, M=40 dopants, X=1,2,3,4)
- We found a split in scaling relationship between ΔG_{O^*} vs ΔG_{OH^*} .
 - Dopants with a slope of 1 do not obey the d-band center model for adsorption
 - Results in a shift in theoretical η_{OER}^{Th} and change in selectivity
- Si, Fe, Zr, Rh, Mn, Ir, and Hf are ideal for CER via the ClO^* precursor.



Acknowledgements



Funding and Support



Supercomputing resources



The Computational Catalysis and Interface Chemistry Group



Lars Grabow



Najmeh Honari



Hong Zhong





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CHEMICAL ENGINEERING REIMAGINED

Thank you!

Questions?